

# Thermal Abuse Simulation in a Battery

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# / Agenda

- What is thermal abuse?
- Objectives of simulation
- Components (Models)
- Results

# What is thermal abuse?

Video found at <https://www.ibtimes.com/tesla-news-model-s-crashes-tow-truck-russia-injuring-three-people-2812133>

- **Exothermic** reaction within a battery cell
- Can quickly **propagate** to neighbor cells
- Does not need air to burn, hard to extinguish
- Can start by
  - Nail penetration
  - Internal short (dendrith growth)
  - External short
  - Crash
  - Thermal failures

<https://www.ibtimes.com/tesla-news-model-s-crashes-tow-truck-russia-injuring-three-people-2812133>

# Objectives of simulation

- Does thermal runaway propagate to neighbor cells?
- How quickly does the propagation take place?
- Identify critical cells for start of thermal runaway
  - Reduce number of experiments
- What temperatures are reached, how much gas is released under what temperature and pressure?

# / Components

- Nail model: Initiate the thermal runaway (in the lab, as a failure in the field)
- Internal short propagation (first mode of heat production)
- Thermal abuse model (1-eqn or NREL 4-eqn model)
- Gas release model
- Chemical reactions in gas/air mixture
- Boiling model of cooling liquid
- Particle release
- Damage modeling
  - Irreversible foam change
  - Melting
  - Deformation

# Components

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- Internal short propagation (first mode of heat production)
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- Gas release model
- Chemical reactions in gas/air mixture
- Boiling model of cooling liquid
- Particle release and tracking
- Damage modeling
  - Irreversible foam change
  - Melting
  - Deformation

Today's talk, Workshop on ALH

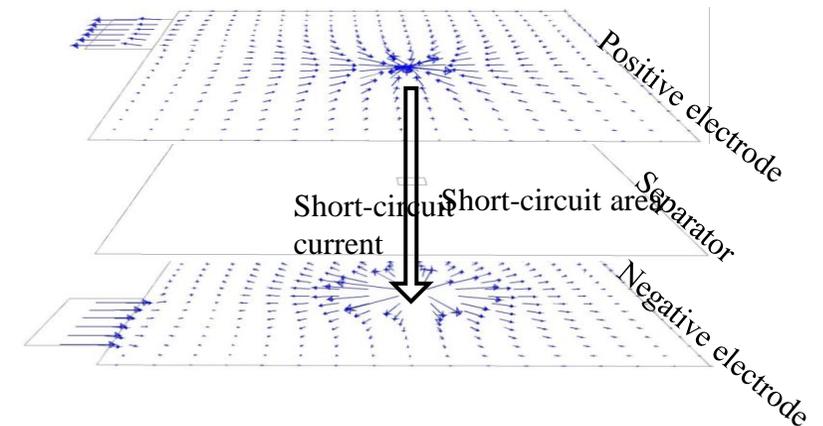
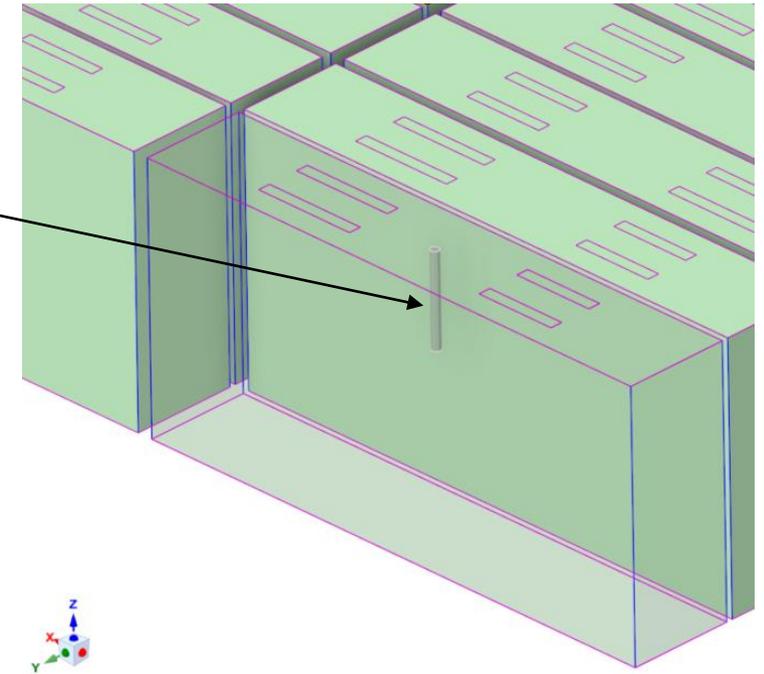
Possible, but not tested yet for this application

# / Components

- **Nail model**: Initiate the thermal runaway (in the lab, as a failure in the field)
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# Nail model

- Prepare in the battery geometry a small cylindrical region
- 2 different methods available:
  - Heat source method
    - Apply for some time a heat source. Usually try and error to determine magnitude and duration. „just enough to start the thermal runaway“
  - Specify internal short resistance
    - Would take into account the SOC
    - Non-trivial to find correct resistance
    - Requires to run dual-potential MSMD battery model



# / Components

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# Internal short propagation

- Electric separator fails at temperatures lower than thermal abuse reactions
- Electric energy converted depends on (local) SOC
- Recommended: Reaction rate model (a 5th reaction similar to NREL 4 eqn model)
  - Does not require dual-potential MSMD model
  - Very efficient

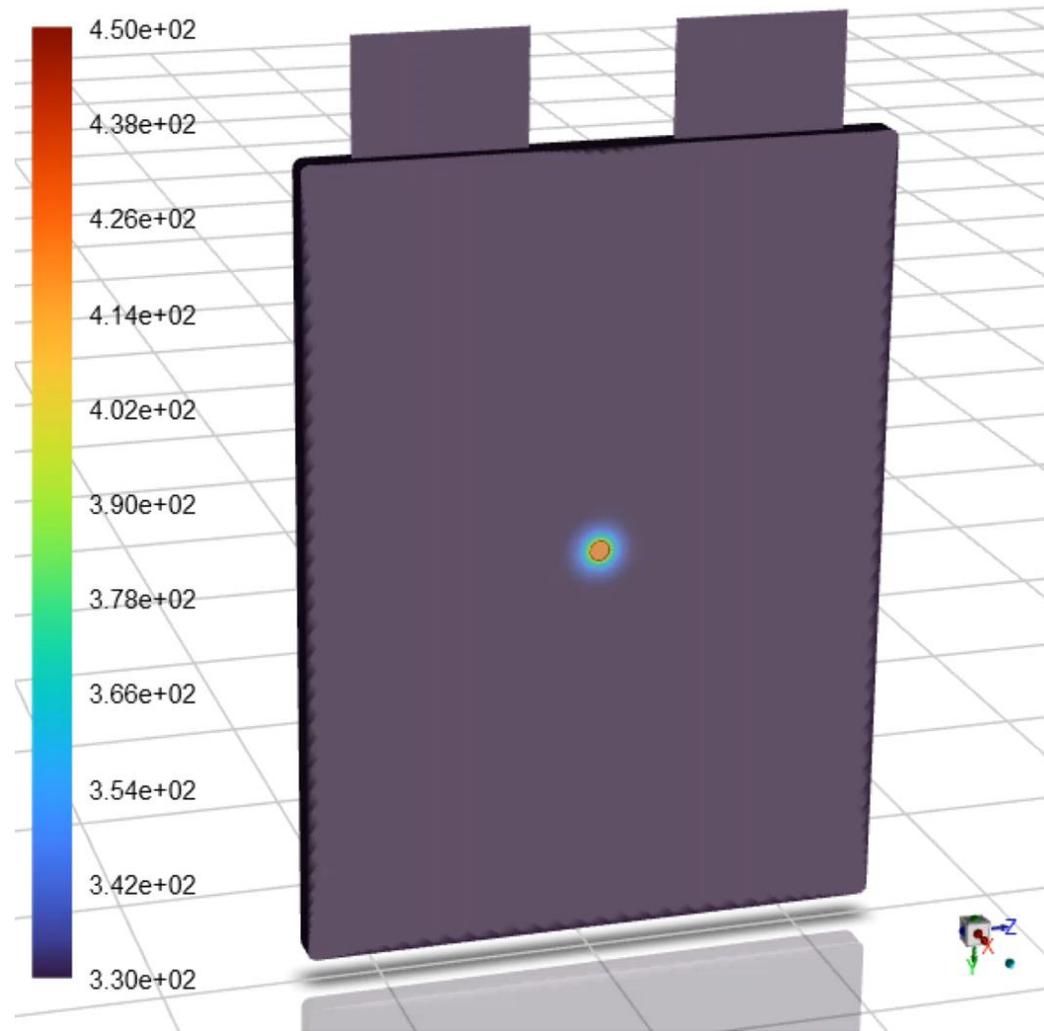
$$R_{sh}(T, SoC) = ISC_{cond} \times A_{ec} \times \exp\left(-\frac{E_{ec}}{R_u T}\right) \times SoC$$

$$\frac{dSoC}{dt} = -R_{sh}$$

$$S_{ec} = H_{ec} \times R_{sh}$$

P. T. Coman, E. C. Darcy, C. T. Veje, and R. E. White, "Modelling Li-Ion Cell Thermal Runaway Triggered by an Internal Short Circuit Device Using an Efficiency Factor and Arrhenius Formulations", J. of the Electrochemical Society, 164 (4) A587-A593 (2017).

# Case03 – Short Propagation Animation



# / Components

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# Introduction of Battery Thermal Abuse Models

- Reaction kinetics are used to model the decomposition reactions.
- Two models have been implemented in both Twin Builder and Fluent
  - **One-equation model**
    - D. D. MacNeil, J. R. Dahn, “Test of Reaction Kinetics Using Both Differential Scanning and Accelerating Rate Calorimetries as Applied to the Reaction of  $\text{LiCoO}_2$  in Non-aqueous Electrolyte”, J. Phys Chem., 2001.
  - **NREL’s four-equation model**
    - T. D. Hatchard, D. D. MacNeil, A. Basu, and J. R. Dahn, “Thermal Model of Cylindrical and Prismatic Lithium-Ion Cells”, J. of the Electrochemical Society, 2001.
    - Gi-Heon Kim, Ahmad Pesaran, Robert Spotnitz, “A Three-dimensional thermal abuse model for lithium-ion cells”, J. of Power Resources, 2007.

# 1-Eqn Thermal Abuse Model

- Total heat generation due to thermal abuse can be modeled as one exothermic reaction.

$$S_{abuse\_chem} = S$$

$$R(T, \alpha) = A \times \alpha^m \times (1 - \alpha)^n \times \exp\left(-\frac{E_a}{R_u T}\right)$$

$$S = H \times W \times R$$

$$\frac{d\alpha}{dt} = R$$

where A, m, n, E<sub>a</sub>, H, W are model constants; H specific heat (J/kg);  
W volume specific content (kg/m<sup>3</sup>)

- This is a sub-set of the 4-equ thermal abuse model.

	reaction model	dα/dt =	kα <sup>m</sup> (1-α) <sup>n</sup> (-ln(1-α)) <sup>p</sup>		
			m	n	P
1	one-dimensional diffusion	kα <sup>-1</sup>	-1	0	0
2		kα	1	0	0
3	power law	kα <sup>1/2</sup>	0.5	0	0
4	power law	kα <sup>2/3</sup>	2/3	0	0
5	power law	kα <sup>3/4</sup>	3/4	0	0
6	zero order	k	0	0	0
7	contracting cylinder	k(1-α) <sup>1/2</sup>	0	0.5	0
8	contracting sphere	k(1-α) <sup>2/3</sup>	0	2/3	0
9	first order (n <sup>th</sup> order)	k(1-α)	0	1	0
10	second order (n <sup>th</sup> order)	k(1-α) <sup>2</sup>	0	2	0
11	Avrami-Erofeev	k(1-α)(-ln(1-α)) <sup>1/2</sup>	0	1	0.5
12	Avrami-Erofeev	k(1-α)(-ln(1-α)) <sup>2/3</sup>	0	1	2/3
13	Avrami-Erofeev	k(1-α)(-ln(1-α)) <sup>3/4</sup>	0	1	3/4
14	autocatalytic	kα(1-α)	1	1	0
15	two-dimensional diffusion	k(-ln(1-α)) <sup>-1</sup>	0	0	-1
16	diffusion controlled	k(1-(1-α) <sup>1/3</sup> ) <sup>-1</sup> (1-α) <sup>2/3</sup>			
17	diffusion controlled	k((1-α) <sup>-1/3</sup> -1) <sup>-1</sup>			

D. D. MacNeil, J. R. Dahn, "Test of Reaction Kinetics Using Both Differential Scanning and Accelerating Rate Calorimetries as Applied to the Reaction of Li<sub>x</sub>CoO<sub>2</sub> in Non-aqueous Electrolyte", J. Phys Chem., 2001.

# NREL's 4-Equ Thermal Abuse Model

Table 1. Abuse reactions included in NREL's abuse reaction kinetics model

Reaction #	Reaction	Possible Onset Temperature (°C)
1	Solid Electrolyte Interphase (SEI) layer decomposition	80
2	Anode — electrolyte	100
3	Cathode — electrolyte	130
4	Electrolyte decomposition	180

$$S_{abuse\_chem} = S_{sei} + S_{ne} + S_{pe} + S_{ele}$$

$$R_{sei}(T, c_{sei}) = A_{sei} \times \exp\left(-\frac{E_{a,sei}}{R_u T}\right) \times c_{sei}^{m_{sei}}$$

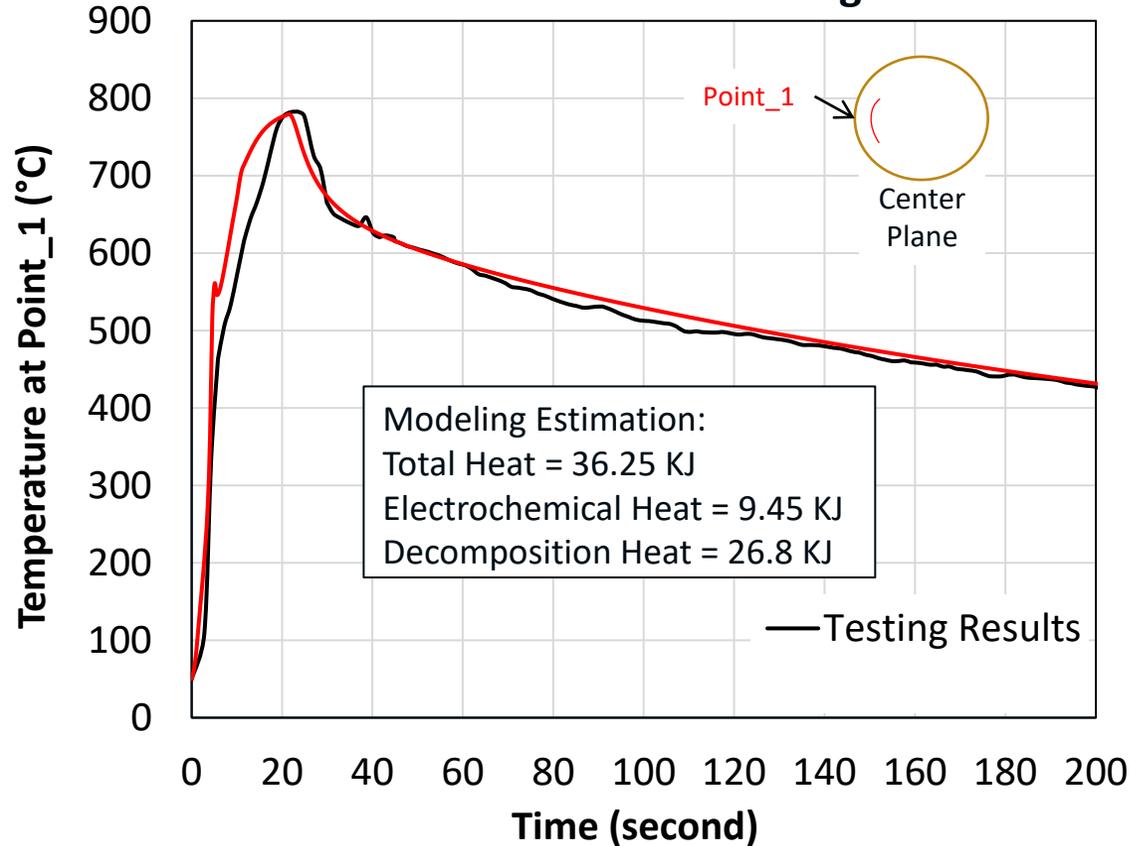
$$S_{sei} = H_{sei} \times W_c \times R_{sei}$$

$$\frac{dc_{sei}}{dt} = -R_{sei}$$

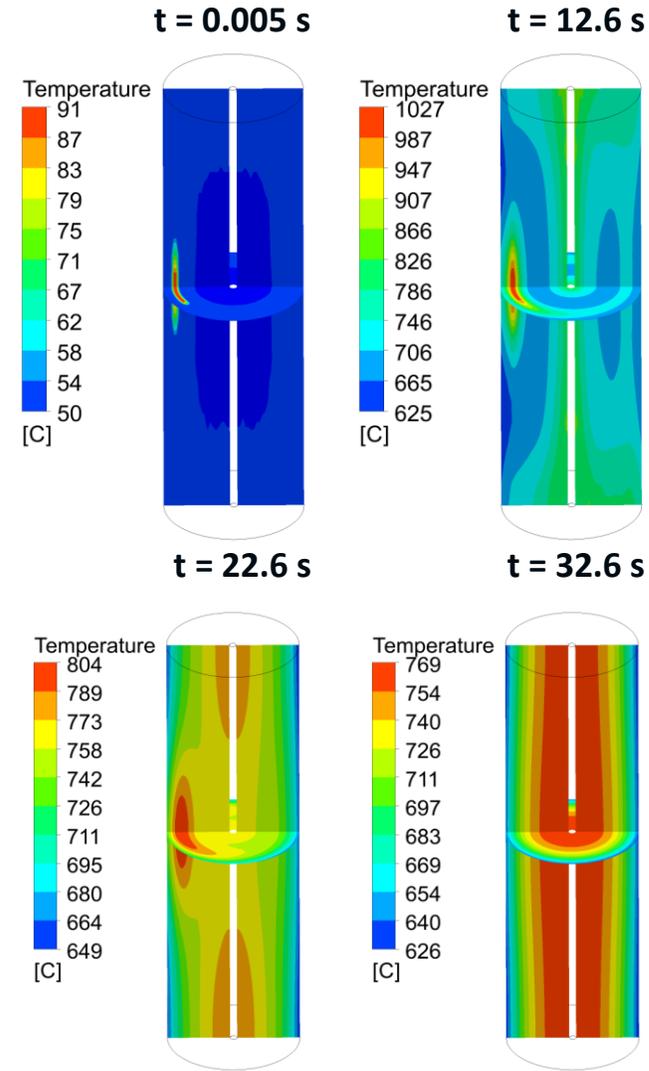
Gi-Heon Kim, Ahmad Pesaran, Robert Spotnitz, "A Three-dimensional thermal abuse model for lithium-ion cells", J. of Power Resources, 2007.

# Cell Thermal Runaway Validation

Simulation Vs. Testing



- The thermal conductivity within battery cell is anisotropy, which is 27 W/m-K, 27 W/m-K and 0.8 W/m-K in axial, azimuthal and radial directions, respectively
- Heat transfer rate along azimuthal and axial directions is faster than radial direction

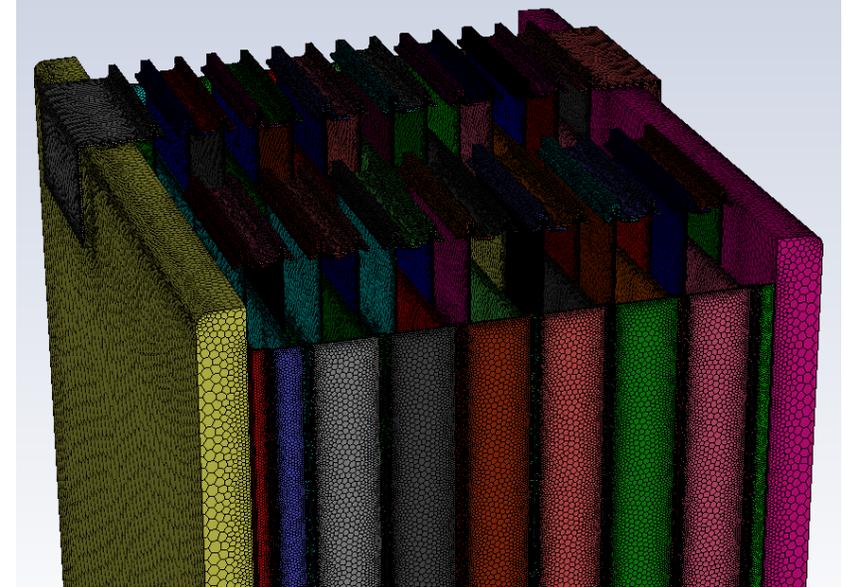
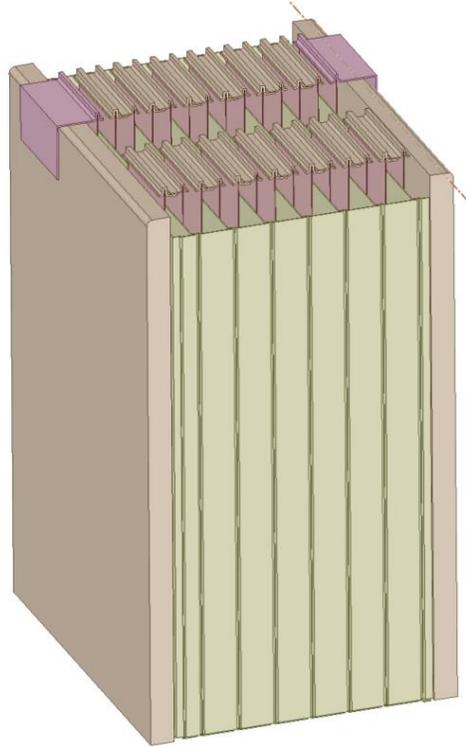
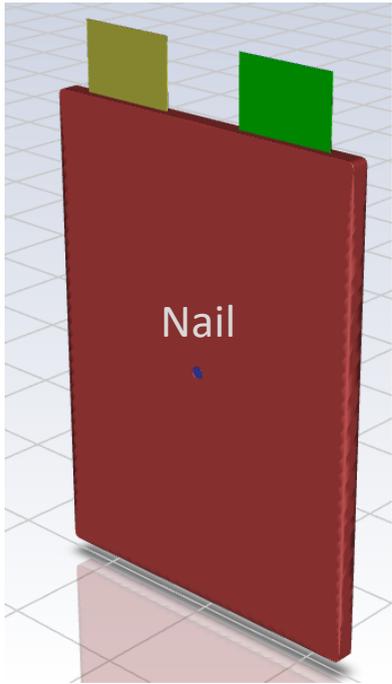


1. "Numerical Investigation of Thermal Runaway Propagation Induced By Internal Short Circuits in a Li-Ion Battery Module", 231st ECS Meeting, New Orleans, LA, May 2017.



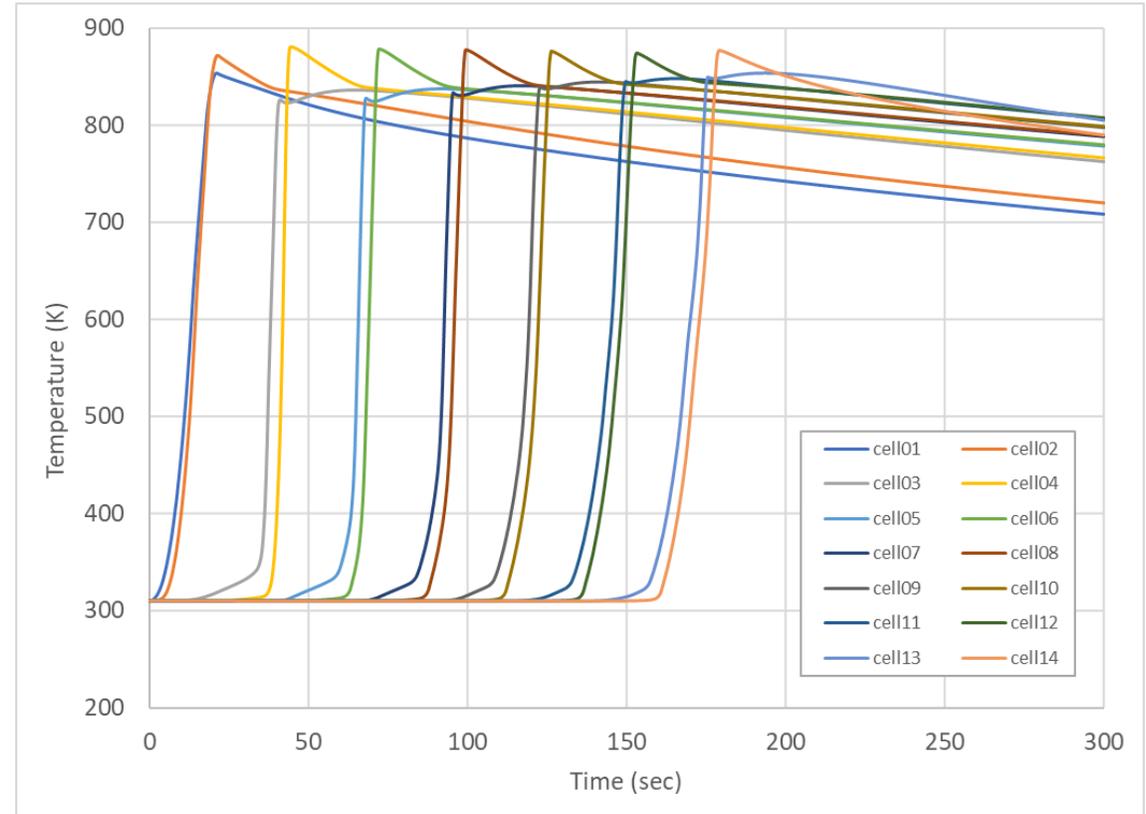
# ALH Tutorial

- The thermal runaway propagation will be performed on a module of 14 cells.
  - The nail region is at the center of the first cell.
- The geometry and the mesh is shown here.
  - The module mesh consists of 4.0 M polyhedral cells.

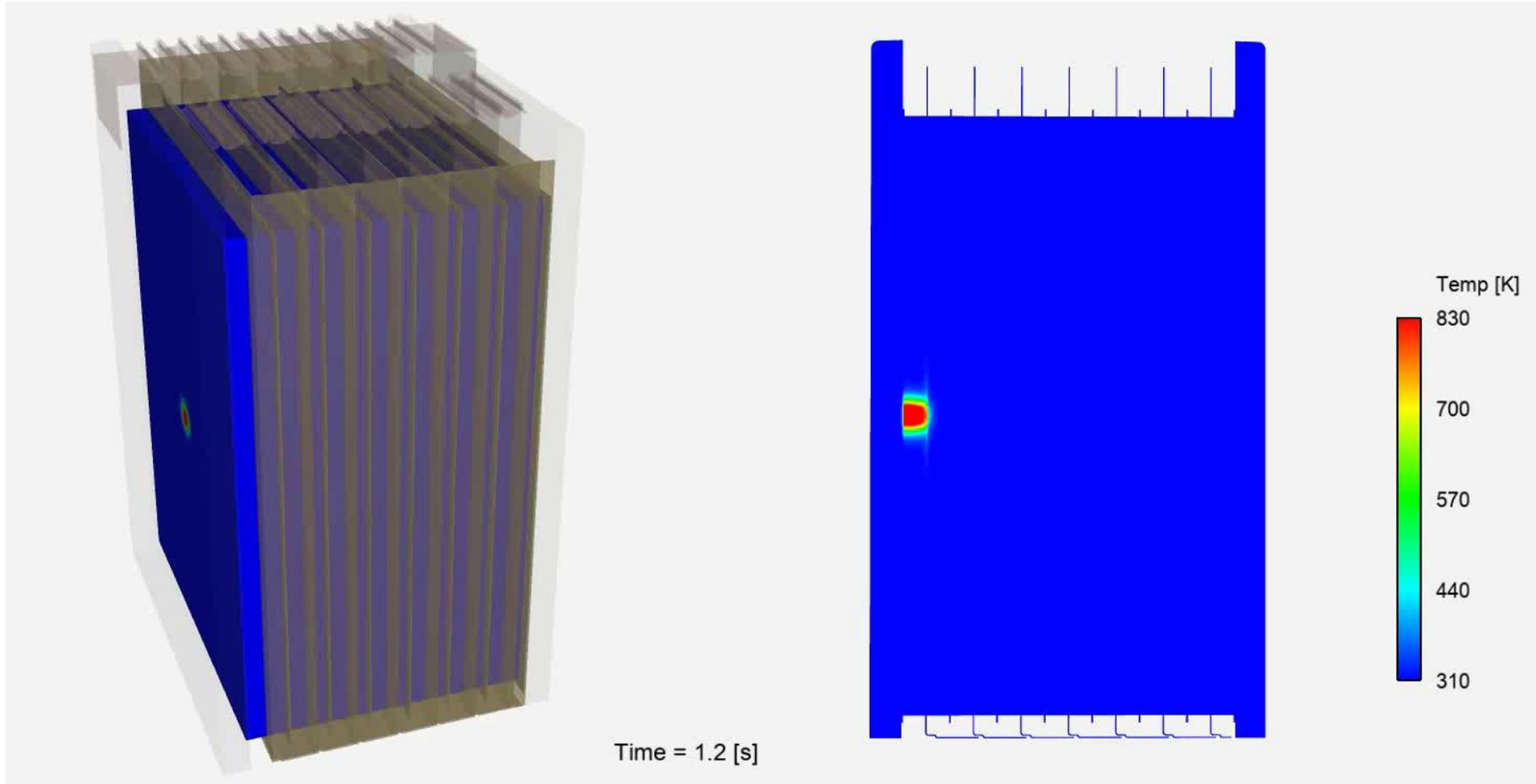


# Thermal Runaway Propagation

- 14 cells in the module
- A pair of two cells shares a cooling fin.
- Thermal runaway propagates from one pair of cells to another.
- One of the design goals is to prevent such propagation.



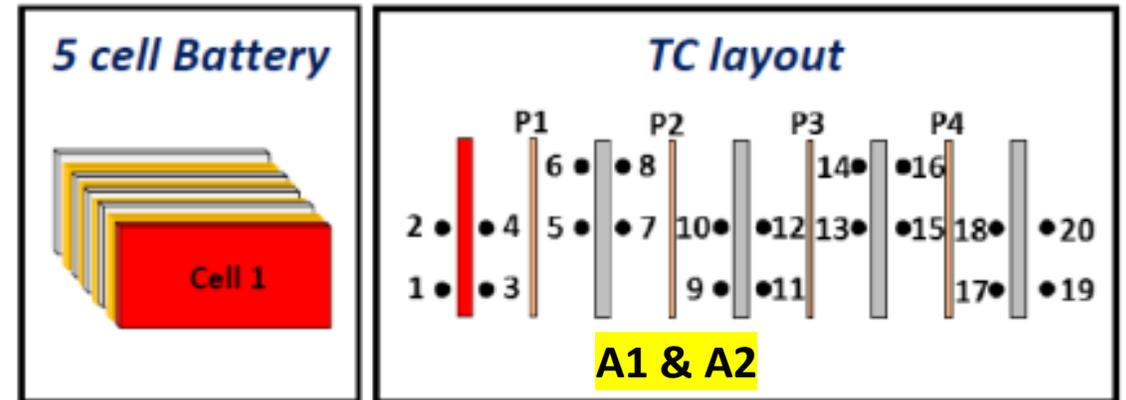
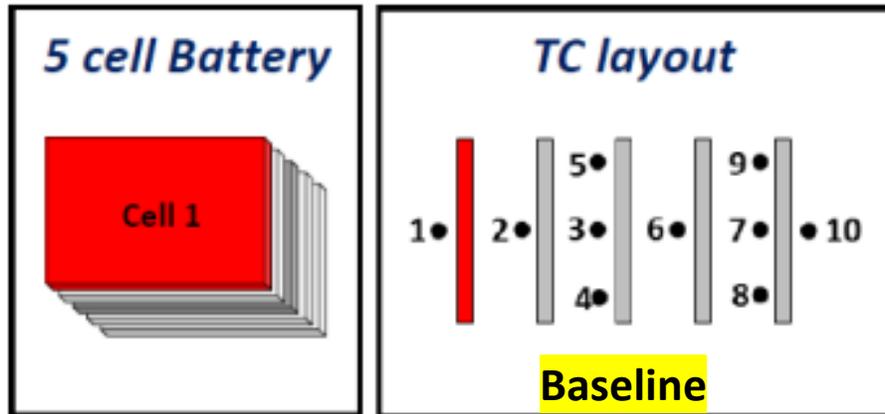
# Thermal Runaway Animation



# Thermal Runaway Propagation Validation



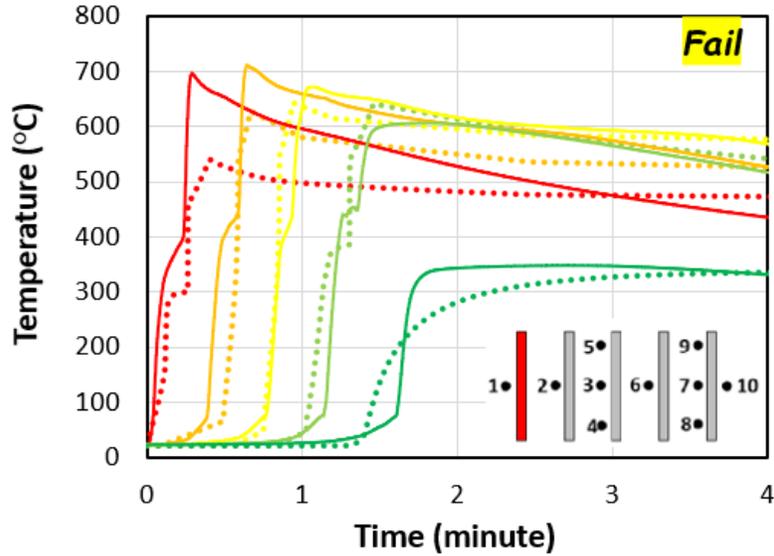
Case No.	Testing Description
Baseline	No thermal management
A1	3.2 mm Al plates between Cells
A2	0.8 mm Al plates between Cells



2. Q Li, CB Yang, S. Santhanagopalan, K. Smith, J. Lamb, L. Steele, L. Torres-Castro, "Numerical Investigation of Thermal Management for Lithium-ion Battery Pack under Thermal Abuse Condition, J. Power Sources 429 (2019) 80-88

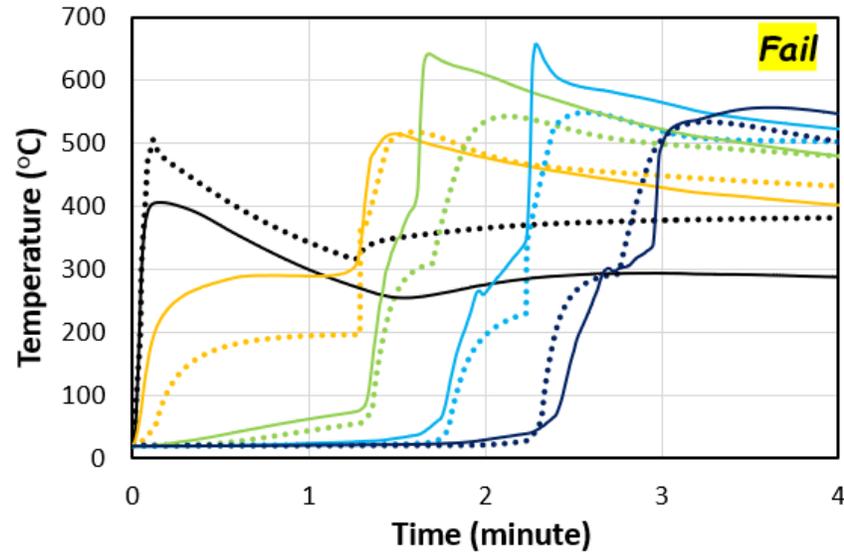
# Thermal Runaway Propagation Validation

Case – Baseline ( $\theta=0$  mm)



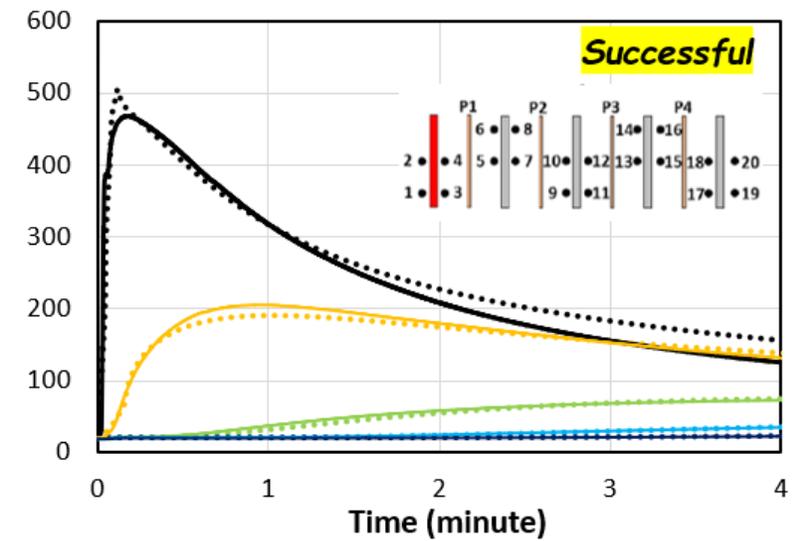
Baseline

Case – A2 ( $\theta=0.8$  mm)



0.8 mm Al-sheet

Case – A1 ( $\theta=3.2$  mm)



3.2 mm Al-sheet

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## / Gas release (venting) model

- The released gas has properties of **hot air**, but is traced as venting-gas, which allows to determine an air to venting-gas ratio in the domain
  - The assumption is that all **oxygen in the battery** is very quickly replaced or consumed
- The total **amount** of gas set free for each cell is **user supplied**
- The current **mass flow rate** of gas is calculated from the **rate of change of the electrolyte reaction** in the corresponding active cell zone
- The temperature of the hot air is the **average cell temperature**
- The best run-time performance of this is obtained by using a user defined function (**UDF**)

# / Components

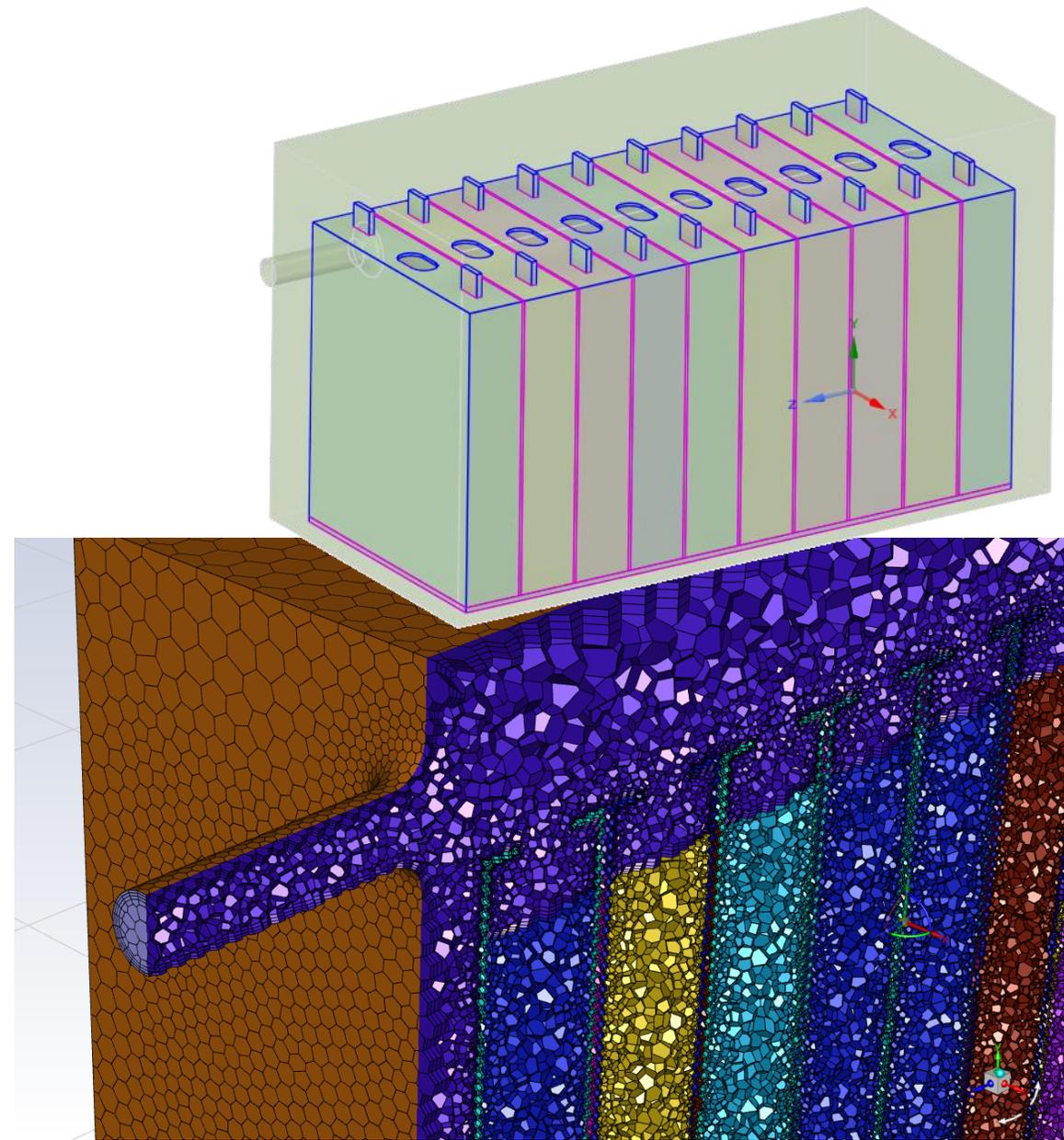
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# / Foam destruction

- Foam is transformed to a coal like solid
- If  $T > 200^{\circ}\text{C}$ , foam gets permanently a higher thermal conductivity
- State is tracked in User Defined Memory (UDM), property of each finite-volume cell
- Implemented as a User Defined Function (UDF)

# New tutorial on ALH

- Uses all features presented so far
  - Initiate thermal runaway with nail region
  - Internal short circuit propagation
  - NREL 4-eqn model
  - Gas release
  - Irreversible foam change
- 10 prismatic battery cells
- 3.3 mio prism polyhedra cells
- Time step 0.025 s, 800 time steps, 20 s total
- 21 h on 32 cores
- Overnight on 128 cores



# Thermal Abuse Model

Battery Model

Enable Battery Model

Model Options | Conductive Zones | Electric Contacts | Model Parameters | UDF | **Advanced Options**

Battery Pack Builder...  
Battery ROM Tool Kit...

Thermal Abuse Model

One-Equation Kinetics Model  Four-Equation Kinetics Model

Material Name: **Li1.1<Ni1/3Co1/3Mn1/3>0.9O2** Material Database

**SEI Decomposition Reaction**

A_sei (e10*1/s)	166700	E_sei (J/mol)	135080	m_sei (-)	1
H_sei (J/g)	257	W_sei (g/m3)	610400	c_sei0 (-)	0.15

**Negative-Solvent Reaction**

A_ne (e10*1/s)	2500	E_ne (J/mol)	135080	m_ne (-)	1
H_ne (J/g)	1714	W_ne (g/m3)	610400	c_neg0 (-)	0.75
t_sei,ref (-)	0.033	t_sei0 (-)	0.033		

**Positive-Solvent Reaction**

A_pe (e10*1/s)	22500	E_pe (J/mol)	154000	m_pe1 (-)	1
H_pe (J/g)	790	W_pe (g/m3)	1293000	m_pe2 (-)	1
alpha0 (-)	0.04				

**Electrolyte Decomposition Reaction**

A_e (e10*1/s)	5.14e+15	E_e (J/mol)	274000	m_e (-)	1
H_e (J/g)	155	W_e (g/m3)	406900	c_e0 (-)	1

Enable Internal Short Heat

**Internal Short Heat Reaction**

A_ec (e10*1/s)	337	E_ec (J/mol)	95150	H_ec (J/m3)	6.12e+08
T_trigger (K)	330	SOC (-)	1		

OK Init Reset Apply Cancel Help

Mass-Flow Inlet

Zone Name: cell-01-fluid\_air

Momentum | **Thermal** | Radiation | Species | DPM | Multiphase | Potential | UDS

Reference Frame: Absolute

Mass Flow Specification Method: Mass Flow Rate

Mass Flow Rate: **udf massflow\_profile::libudf**

Supersonic/Initial Gauge Pressure [Pa]: 0

Direction Specification Method: Normal to Boundary

**Acoustic Wave Model**

Off  
 Non Reflecting  
 Impedance  
 Transparent Flow Forcing

**Turbulence**

Specification Method: Intensity and Viscosity Ratio

Turbulent Intensity [%]: 5

Turbulent Viscosity Ratio: 10

Apply Close Help

# Poron with non-reversible material property

- Activate 1 user defined memory (UDM)
- Hook UDF for thermal conductivity

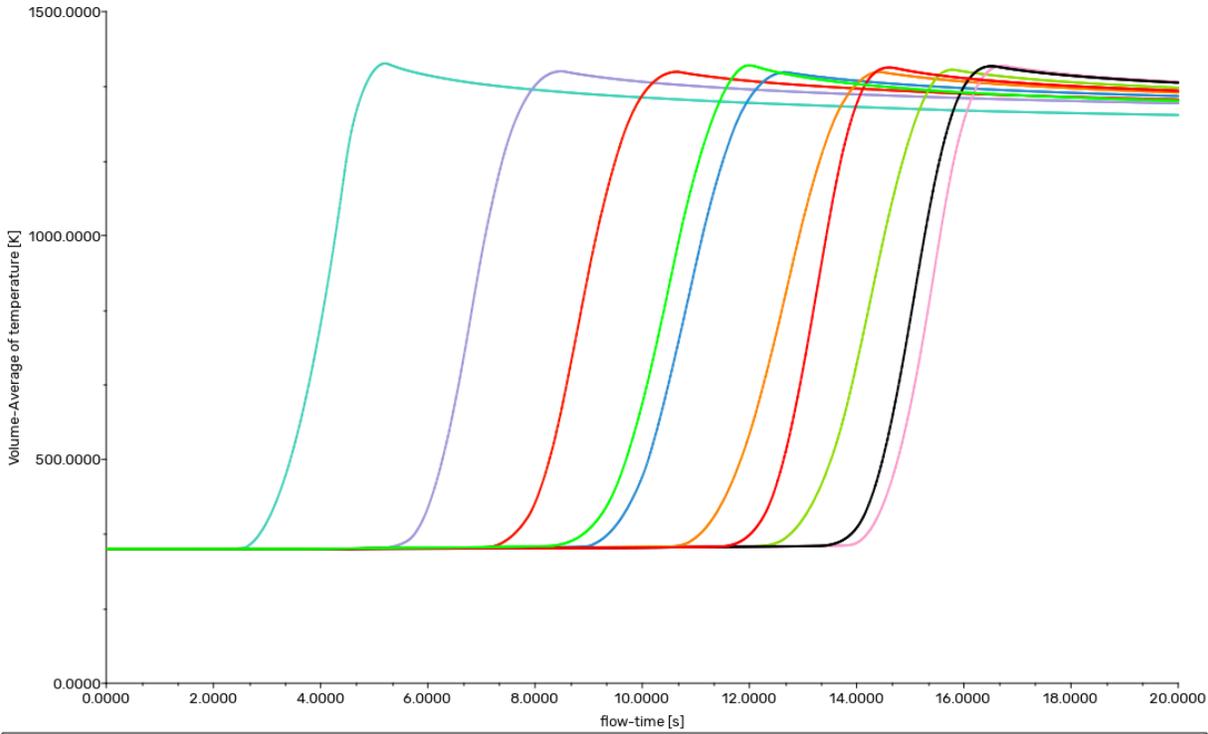
The screenshot shows the 'Create/Edit Materials' dialog box in ANSYS. The material name is 'poron' and the material type is 'solid'. The 'User-Defined Solid Materials' dropdown is set to 'poron' and the 'Mixture' dropdown is set to 'none'. The 'Order Materials by' section has 'Name' selected. The 'Properties' section shows the following settings:

Property	Value	Action
Density [kg/m <sup>3</sup> ]	constant 300	Edit...
Cp (Specific Heat) [J/(kg K)]	constant 1	Edit...
Thermal Conductivity [W/(m K)]	user-defined poron_thermal_conductivity::libudf	Edit...

At the bottom of the dialog, there are buttons for 'Change/Create', 'Delete', 'Close', and 'Help'.

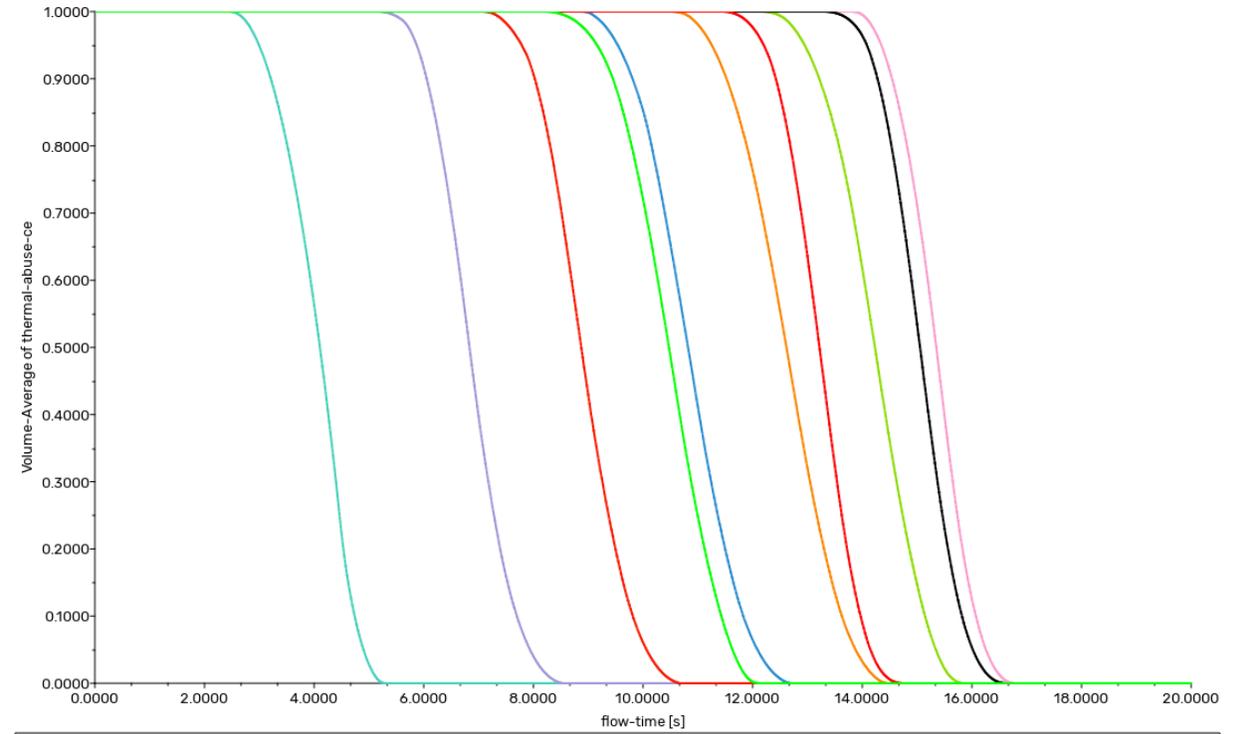
# Monitors

temperatures-rplot (Time=2.0000e+01 s)



temperatures(cell-01) temperatures(cell-02) temperatures(cell-03) temperatures(cell-04) temperatures(cell-05) temperatures(cell-06) temperatures(cell-07)

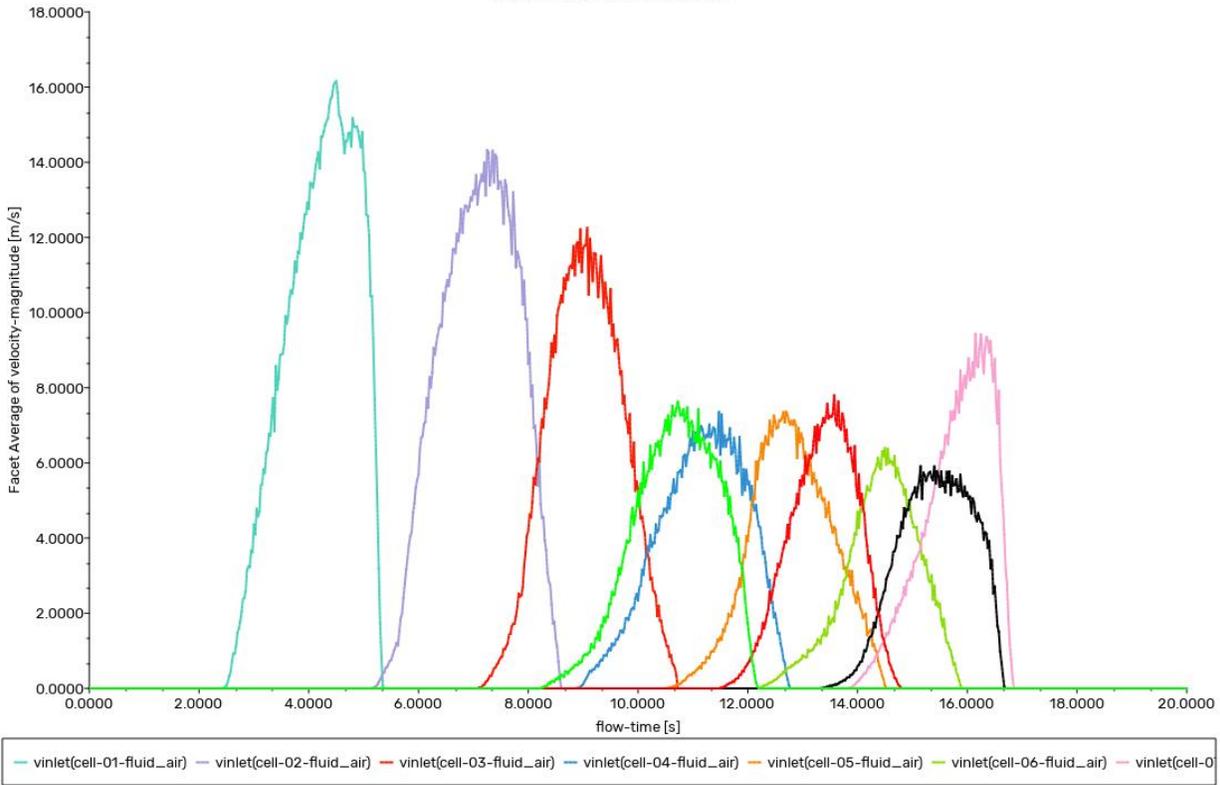
ce-rplot (Time=2.0000e+01 s)



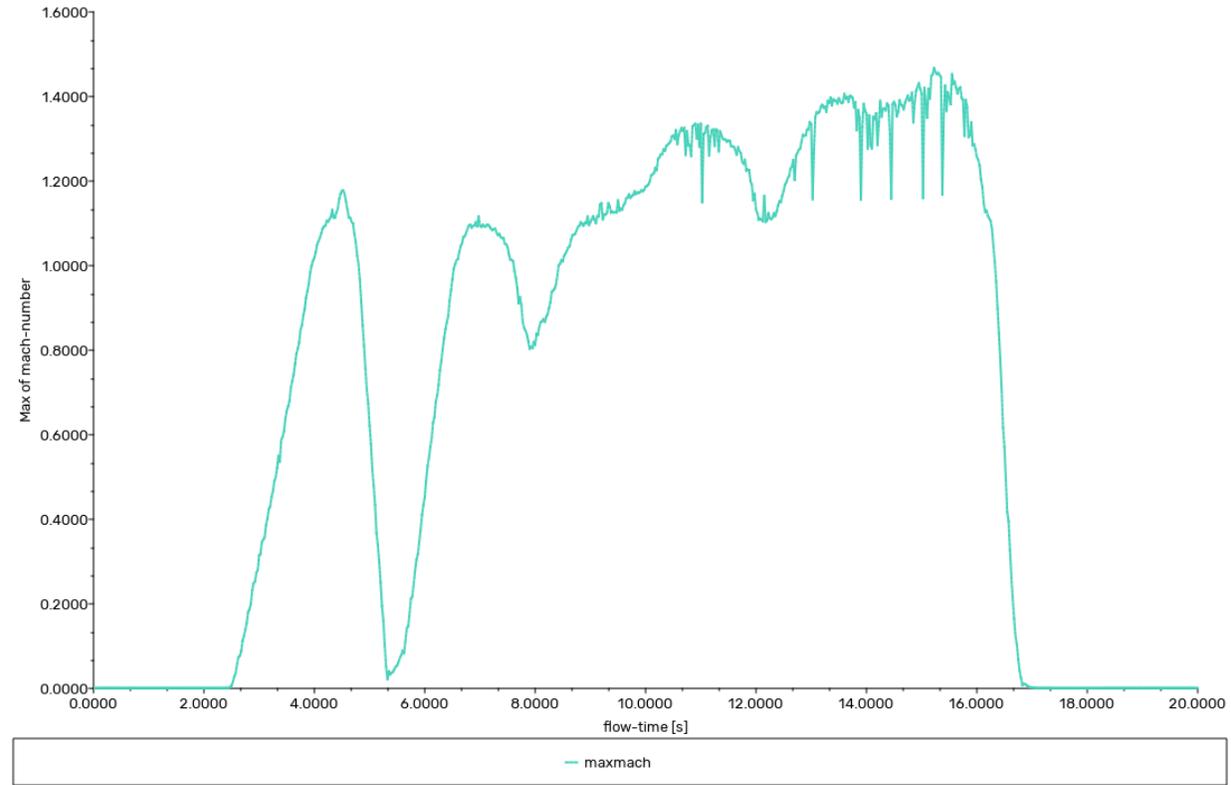
ce(cell-01) ce(cell-02) ce(cell-03) ce(cell-04) ce(cell-05) ce(cell-06) ce(cell-07) ce(cell-08) ce(cell-09) ce(cell-10)

# Monitors

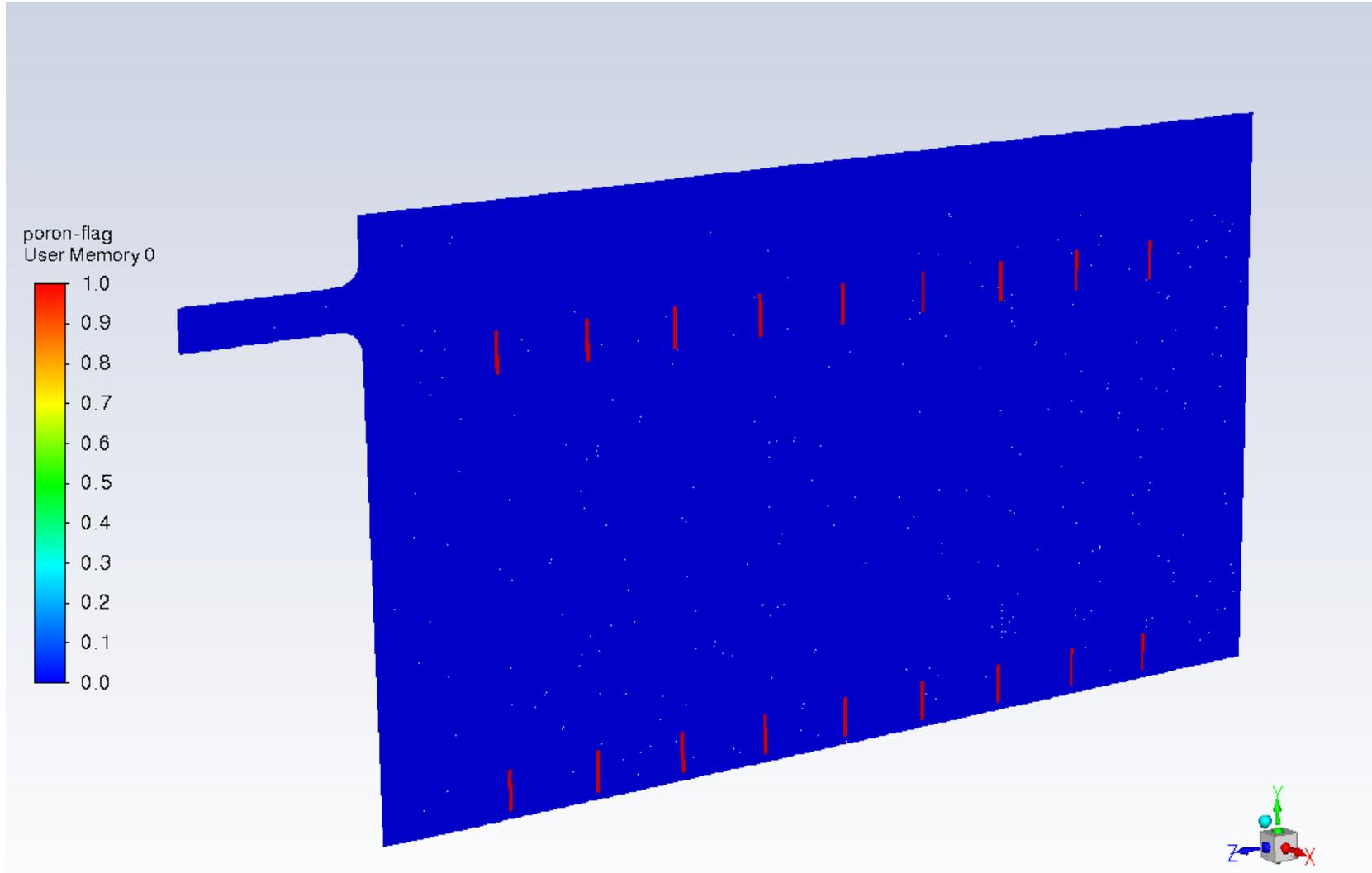
vinlet-rplot (Time=2.0000e+01 s)



maxmach-rplot (Time=2.0000e+01 s)

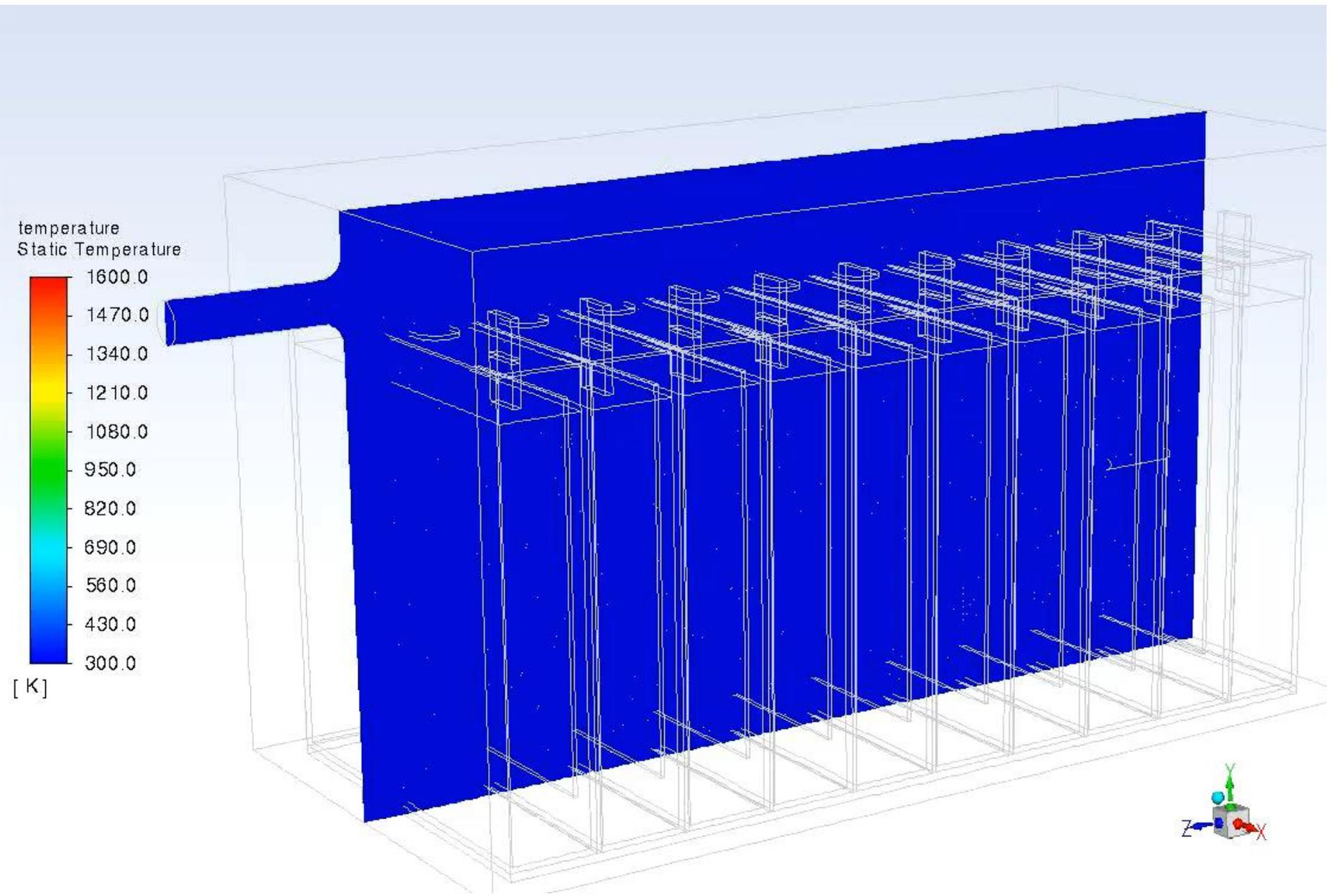


# Poron non-reversible change



The flag for poron change is activated in all 9 regions

# Animation



# Manage Thermal Runaway

## Customer Goals

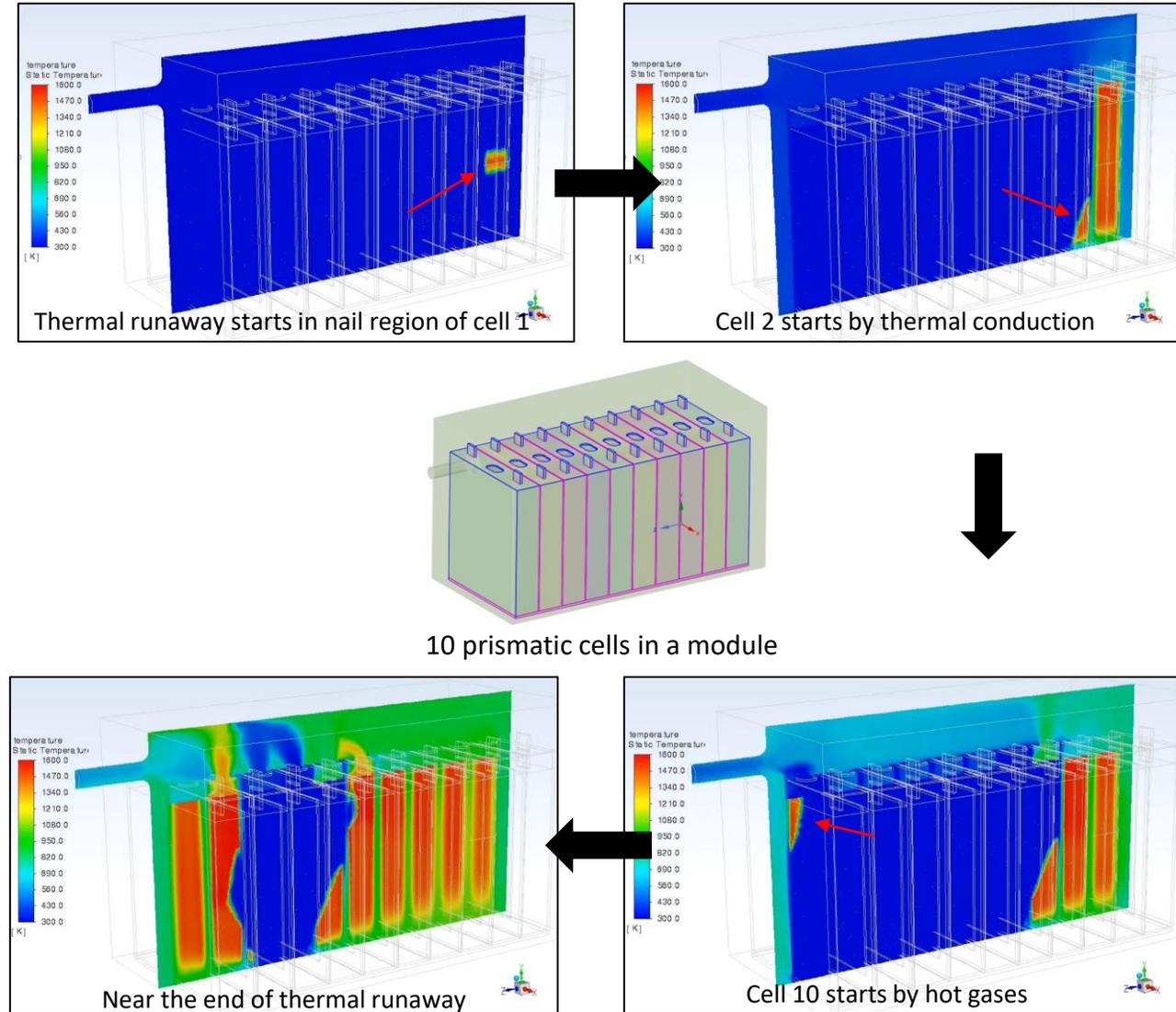
- Ensure that a **thermal runaway event will stay within regulatory limits.**
- **Reduce development time and costs** by replacing expensive measurements with simulation.

## Solution

- **Heat sources and thermal conduction are modeled with build-in models of Ansys Fluent**
- **Gas release from cells is captured with a UDF** which relates the reaction progress in each cell with a mass flow inlet at the venting holes of the cells

## Benefits

- **Tracing the hot gases** within the battery will **capture a heat transfer mechanism** that is very important in some designs
- **Experimental testing is very expensive** as the prototypes will be destroyed in due process and lab needs special fire protection
- **Gain insight to design heat shields, heat capacities, and flow guides.**



# Appendix

# / A thought about experiments

- How good are experiments in reproducing the time to thermal runaway? In the sense of taking 10 new cells of the same kind and bringing them to thermal runaway. What would be the distribution of times measured?